

Séminaire LMT – 21 février 2013

Lagrange-remap solver and low-diffusive interface capturing for air-water flows

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Outline

1. Context, applications
2. System derivation
3. Numerical method
4. Antidiffusive procedure for the gas-liquid interface
5. Numerical experiments & validation
6. Concluding remarks

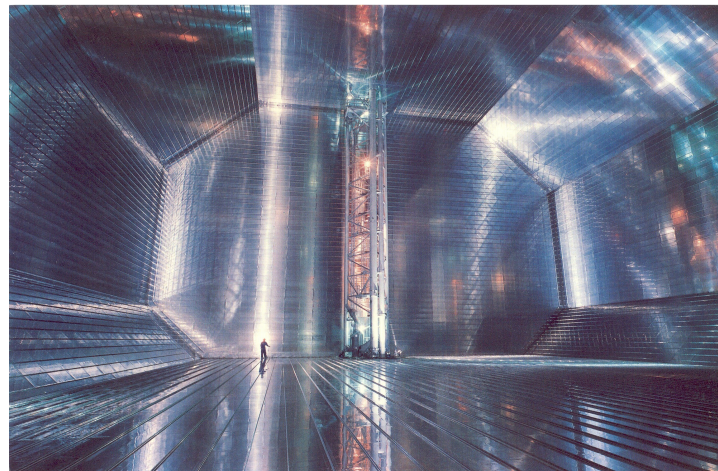
Context, applications

- Air-water flows, violent flow conditions
- Fast dynamics, transient regime
- Applications : Liquified Natural Gas LNG carriers, hydrodynamics, coastal engineering, wave impact, ...

Wave impact pressure peak analysis



LNG carrier tank



Objectives

- Design numerical methods subject to some requirements :
 - Robustness
 - Accuracy
 - Conservation
 - Fluid treated as compressible
 - **Natural parallel extension / implementation**
- Accelerate computations to 2 or 3 orders of magnitude, allowing for statistics (as for experimental setups, hexapods)

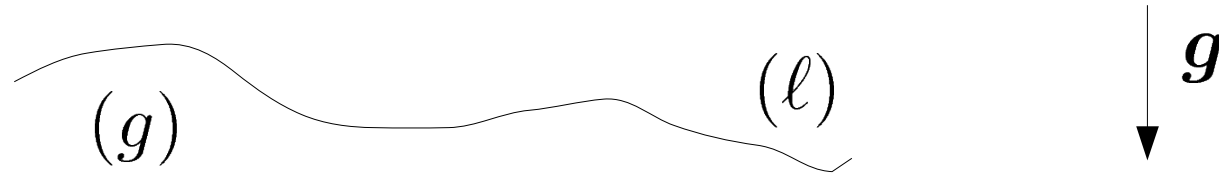
Sources of stiffness

- Gas/liquid mass density ratio of order 1000
- Stiffness due to weak compressibility of liquid → low Mach number flows
- Gas-liquid free boundaries

Assumptions here

- Viscous effects omitted
- Surface tension omitted

Derivation of the system (inviscid)



$$\partial_t \rho_k + \nabla \cdot (\rho_k \mathbf{u}) = 0$$

$$\partial_t (\rho_k \mathbf{u}) + \nabla \cdot (\rho_k \mathbf{u} \otimes \mathbf{u}) + \nabla p = \rho_k \mathbf{g}, \quad k = g, \ell$$

Indicator function : $z = z(\mathbf{x}, t) \in \{0, 1\}$ $\rho = z\rho_g + (1 - z)\rho_\ell$

$$\partial_t \rho + \nabla \cdot (\rho \mathbf{u}) = 0,$$

$$\partial_t (\rho \mathbf{u}) + \nabla \cdot (\rho \mathbf{u} \otimes \mathbf{u}) + \nabla p = \rho \mathbf{g},$$

$$D_t z = \partial_t z + \mathbf{u} \cdot \nabla z = 0,$$

$$p = z p_\ell(\rho_\ell) + (1 - z) p_g(\rho_g)$$

$$\frac{\partial p_k}{\partial \rho_k} = c_k^2 > 0$$

Involving gas mass fraction

$$c_g \in \{0, 1\}$$

$$\partial_t(c_g \rho) + \nabla \cdot (c_g \rho \mathbf{u}) = 0$$

From

$$\partial_t \rho + \nabla \cdot (\rho \mathbf{u}) = 0,$$

we also get

$$D_t c_g = \partial_t c_g + \mathbf{u} \cdot \nabla c_g = 0.$$

Dealing with numerical z in $[0, 1]$

$$\partial_t \rho + \nabla \cdot (\rho \mathbf{u}) = 0, \quad \text{Total mass conservation}$$

$$\partial_t (\rho \mathbf{u}) + \nabla \cdot (\rho \mathbf{u} \otimes \mathbf{u}) + \nabla p = \rho \mathbf{g}, \quad \text{Momentum balance}$$

$$\partial_t (c_g \rho) + \nabla \cdot (c_g \rho \mathbf{u}) = 0, \quad \text{Gas mass conservation}$$

$$D_t z = \partial_t z + \mathbf{u} \cdot \nabla z = 0,$$

$$p = z p_\ell(\rho_\ell) + (1 - z) p_g(\rho_g) \quad \text{Pressure closure}$$

In the spirit of [Kokh-Lagoutière 2010]

Introducing the volume fraction :

$$z \rho_g = c_g \rho, \quad z \rho_g + (1 - z) \rho_\ell = \rho.$$

Shorcoming: $\rho_g = \frac{c_g \rho}{z}$ may be undetermined numerically.

Use of a (simplified) volume-averaged system and pressure equilibrium closure

$$\partial_t \rho + \nabla \cdot (\rho \mathbf{u}) = 0,$$

$$\partial_t (\rho \mathbf{u}) + \nabla \cdot (\rho \mathbf{u} \otimes \mathbf{u}) + \nabla p = \rho \mathbf{g},$$

$$\partial_t (c_g \rho) + \nabla \cdot (c_g \rho \mathbf{u}) = 0,$$

$$p = p_g(\rho_g) = p_\ell(\rho_\ell) \quad \text{Pressure equilibrium into an elementary volume}$$

can be rewritten as

$$\partial_t (\alpha \rho_g) + \nabla \cdot (\alpha \rho_g \mathbf{u}) = 0,$$

$$\partial_t ((1 - \alpha) \rho_\ell) + \nabla \cdot ((1 - \alpha) \rho_\ell \mathbf{u}) = 0,$$

$$\partial_t (\rho \mathbf{u}) + \nabla \cdot (\rho \mathbf{u} \otimes \mathbf{u}) + \nabla p = \rho \mathbf{g},$$

$$p = p_g(\rho_g) = p_\ell(\rho_\ell)$$

Typical equations of state (EOS) in use

$$p_g(\rho_g) = p_0 \left(\frac{\rho_g}{\rho_g^0} \right)^{\gamma_g}, \quad \gamma_g = 1.4,$$

$$p_l(\rho_l) = p_0 + \frac{\rho_l^0 c_s^2}{\gamma_l} \left(\left(\frac{\rho_l}{\rho_l^0} \right)^{\gamma_l} - 1 \right), \quad \gamma_l = 7.$$

Near atmospheric conditions :

$$p_0 = 10^5 \text{ Pa}, \quad \rho_g^0 = 1.2 \text{ kg.m}^{-3}, \quad \rho_l^0 = 1000 \text{ kg.m}^{-3}.$$

$$c_s = 1500 \text{ m.s}^{-1}. \text{ Artificial: } c_s = 350 \text{ m.s}^{-1}.$$

Pressure equilibrium equation

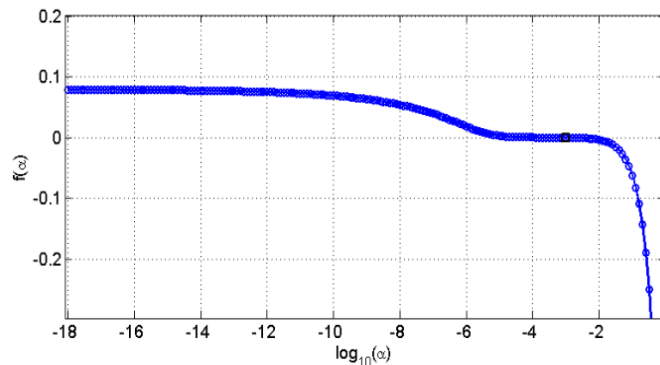
- From the knowledge of the conservative variables $W_g = \alpha \rho_g$ and $W_\ell = (1 - \alpha) \rho_\ell$, we have to solve :

$$p_g(\rho_g) = p_\ell(\rho_\ell)$$

i.e.

$$\varphi(\alpha) = \left(\frac{W_g}{\alpha \rho_g^0} \right)^{\gamma_g} - 1 - K \left[\left(\frac{W_\ell}{(1 - \alpha) \rho_\ell^0} \right)^{\gamma_\ell} - 1 \right] = 0, \quad \alpha \in]0, 1[.$$

- NB : very stiff function, the choice of the iterative solver requires attention (initial guess, surrogates, Newton, etc.)



In fact, there is a trick ... :

Trick for initial guess :

- The liquid mass conservation equation can be written in conservative form as :

$$\partial_t(1 - \alpha) + \nabla \cdot [(1 - \alpha)\mathbf{u}] = -\frac{D_t \rho_\ell}{\rho_\ell}.$$

- Under the *weak compressibility assumption* or the liquid phase, we get

$$\partial_t \alpha + \nabla \cdot (\alpha \mathbf{u}) = 0.$$

- A numerical scheme is applied to this additional "guess equation" to compute initial guesses of the iterative solver
→ Newton algorithm converges in 2 iterates with acceptable accuracy (**strong improvement in CPU time**).

Numerical scheme

Remapped Lagrange Eulerian solver

- First write the equations in **Lagrange** form

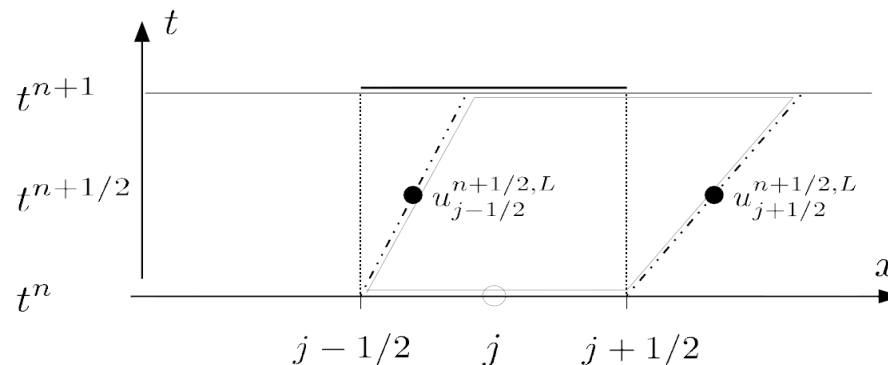
$$\rho D_t \left(\frac{1}{\rho} \right) - \nabla \cdot \mathbf{u} = 0, \quad \frac{d}{dt} \int_{\Omega_t} \alpha \rho_g dx = 0,$$

$$\rho D_t \mathbf{u} + \nabla p = \mathbf{g}, \quad \frac{d}{dt} \int_{\Omega_t} (1 - \alpha) \rho_\ell dx = 0,$$

$$D_t c_g = 0,$$

$$\frac{d}{dt} \int_{\Omega_t} \rho \mathbf{u} dx + \int_{\Omega_t} \nabla p dx = \int_{\Omega_t} \rho \mathbf{g}.$$

- **Advance** in time
- **Project** the quantities on the fixed Eulerian grid (remap)

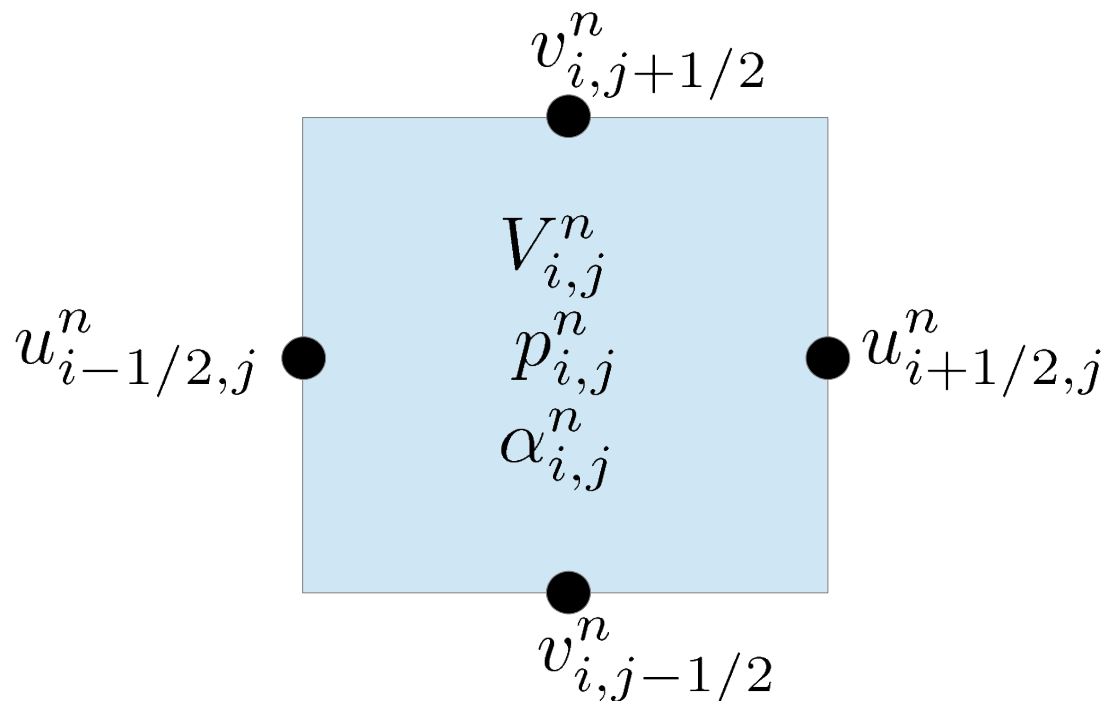


Typical Lagrange scheme (spatial staggered grid)

$$u_{i+1/2,j}^{n+1/2,L} = u_{i+1/2,j}^n - \frac{\Delta t}{2} \frac{\Delta y}{m_{i+1/2,j}^n} \left[(p+q)_{i+1,j}^{n+1/2,L} - (p+q)_{i,j}^{n+1/2,L} \right],$$

$$v_{i,j+1/2}^{n+1/2,L} = v_{i,j+1/2}^n - \frac{\Delta t}{2} \frac{\Delta x}{m_{i,j+1/2}^n} \left[(p+q)_{i,j+1}^{n+1/2,L} - (p+q)_{i,j}^{n+1/2,L} \right] + \frac{\Delta t}{2} g.$$

$$V_{i,j}^{n+1,L} = V_{i,j}^n + \Delta t \Delta y \left(u_{i+1/2,j}^{n+1/2,L} - u_{i-1/2,j}^{n+1/2,L} \right) + \Delta t \Delta x \left(v_{i,j+1/2}^{n+1/2,L} - v_{i,j-1/2}^{n+1/2,L} \right).$$



A short walk on Lagrange-remap (Euler 1D)

Lagrange step :

$$\rho_j^{n+1,L} V_j^{n+1,L} = \rho_j^n V_j^n$$

Pseudo-viscosity

$$V_j^{n+1,L} = V_j^n + \Delta t (u_{j+1/2}^{n+1/2,L} - u_{j-1/2}^{n+1/2,L})$$

$$m_{j+1/2}^n u_{j+1/2}^{n+1,L} = m_{j+1/2}^n u_{j+1/2}^n - \Delta t (\Delta p_{j+1/2}^{n+1/2,L} + \Delta q_{j+1/2}^{n+1/2,L})$$

“ $de + pd\tau$ ”

$$e_j^{n+1,L} = e_j^n - \frac{p_j^{n+1/2,L} + q_j^{n+1/2,L}}{m_j^n} (V_j^{n+1,L} - V_j^n)$$

$$\frac{e_j^{n+1,L} - e_j^n}{\Delta t} + \frac{p_j^{n+1/2,L}}{m_j^n} (u_{j+1/2}^{n+1/2,L} - u_{j-1/2}^{n+1/2,L}) = -\frac{q_j^{n+1/2,L}}{m_j^n} (u_{j+1/2}^{n+1/2,L} - u_{j-1/2}^{n+1/2,L})$$

$$\begin{aligned} q_j^{n+1/2,L} &\propto -(u_{j+1/2}^{n+1/2,L} - u_{j-1/2}^{n+1/2,L}) \\ &= -\beta(\rho c^2)_j^{n+1/2,L} \Delta u_j^{n+1/2,L} \end{aligned}$$

A short walk on Lagrange-remap ...

- Lagrange step : entropy-satisfying
- Projection step : dissipative process due to Jensen's inequality (consider convex entropies)

...

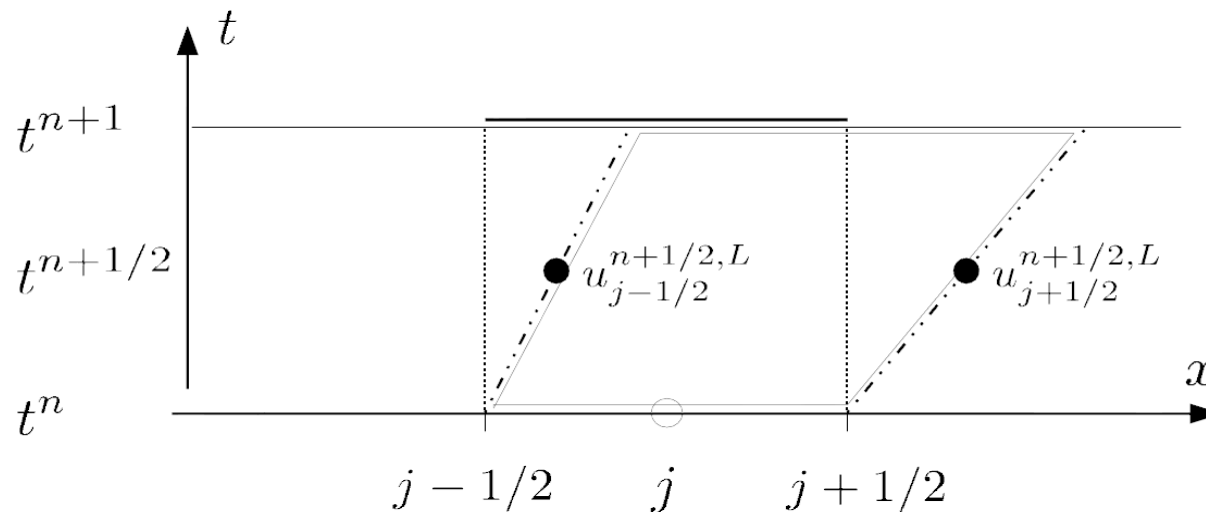
=> rather simple process with positivity & entropy properties, does not require any approximate Riemann solver.

Conservative form

- Lagrange-remap schemes actually can be rewritten in conservative form [De Vuyst et al, preprint 2013].
- 1D case :

$$(\alpha\rho_g)_j^{n+1} = (\alpha\rho_g)_j^{n+1} - \frac{\Delta t}{h} \left[(\Phi_{m,g})_{j+1/2}^{n,n+1} - (\Phi_{m,g})_{j-1/2}^{n,n+1} \right],$$

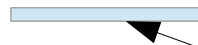
$$(\Phi_{m,g})_{j+1/2}^{n,n+1} = \alpha_{j+1/2}^{n+1,L} (\rho_g)_{j+1/2}^{n+1,L} u_{j+1/2}^{n+1/2,L}$$



Antidiffusive strategy

$$(\alpha\rho_g)_j^{n+1} = (\alpha\rho_g)_j^{n+1} - \frac{\Delta t}{h} \left[(\Phi_{m,g})_{j+1/2}^{n,n+1} - (\Phi_{m,g})_{j-1/2}^{n,n+1} \right],$$

$$(\Phi_{m,g})_{j+1/2}^{n,n+1} = \alpha_{j+1/2}^{n+1,L} (\rho_g)_{j+1/2}^{n+1,L} u_{j+1/2}^{n+1/2,L}$$



Void fraction at interface :
how to compute it ?

- Strategy : « be as most accurate as possible for step-shaped color functions while being stable (just at the limit) »
- Idea : design a combination of **upwind** scheme and **downwind** scheme [Lagoutière Després 2002, Kokh-Lagoutière 2010]
- The advection process can be seen as a over-compressive « limiting » procedure (superbee-like, hyperbee, ...)

Upwinding (stable but diffusive) vs
downwinding (anti-diffusive but unstable) ...

Transport of the mass gas fraction : $\partial_t c_g + \mathbf{u} \cdot \nabla c_g = 0$

- Consistency requirement

$$(c_g)_{i+1/2,j} \in [\min((c_g)_{i,j}, (c_g)_{i+1,j}), \max((c_g)_{i,j}, (c_g)_{i+1,j})]$$

- Stability requirement

« do not produce new extrema, discrete local maximum principle »

- Take the value closest to the downwind one while being in the trust interval.

Some theoretical results

Theorem 4.1. *Under the condition to be respected by the time step (in which $s = \text{sign}(u_{i+1/2}^{n+1/2,L})$)*

$$V_{i+1/2,j,upw}^{n+1,*} - s\Delta t\Delta y u_{i+1/2-s,j} \geq 0, \quad (59)$$

when $u_{i+1/2,j}^{n+1,L} u_{i+s/2,j}^{n+1,L} > 0$ (i.e. when the velocities at the edges of the cell where the stability condition is calculated are of the same sign), the value of $\alpha_{i+1/2,j}^{LowDiff}$ can be taken in the following trust interval I :

$$I = \underbrace{I_1}_{\text{flux consistency for } c_g} \cap \underbrace{I_2^s}_{\text{stability for } c_g} := [\omega_{i+1/2,j}^{n+1,L}, \Omega_{i+1/2,j}^{n+1,L}] \in [0, 1], \quad (60)$$

which is not empty since the upwind value $\alpha_{i+1/2,j,up}^{n+1,L} \in I$, where the interval I_1 are defined by (44) and I_2^s by (48)-(49) (or written in a generic form (C.1)-(C.2)). Moreover, taking $\alpha_{i+1/2,j}^{LowDiff} \in I$ ensures to respect maximum principle on c_g and especially to keep the positivity of the masses of each phases during the projection.

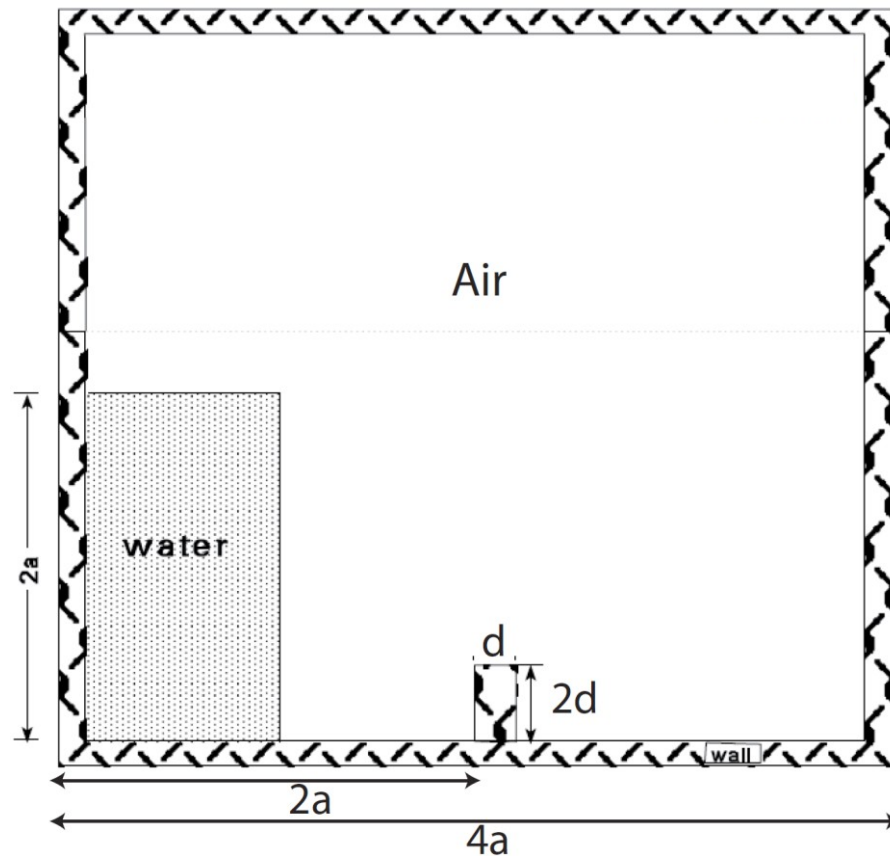
Test cases

and numerical experiments

(+ comparison to physical experiments
for some of them)

1. Collapse of a liquid column with an obstacle

O. Ubbink Numerical prediction of two-fluid systems with sharp interfaces, PhD thesis (1997)



$$a = 0.146 \text{ m}, d = 0.024 \text{ m}$$

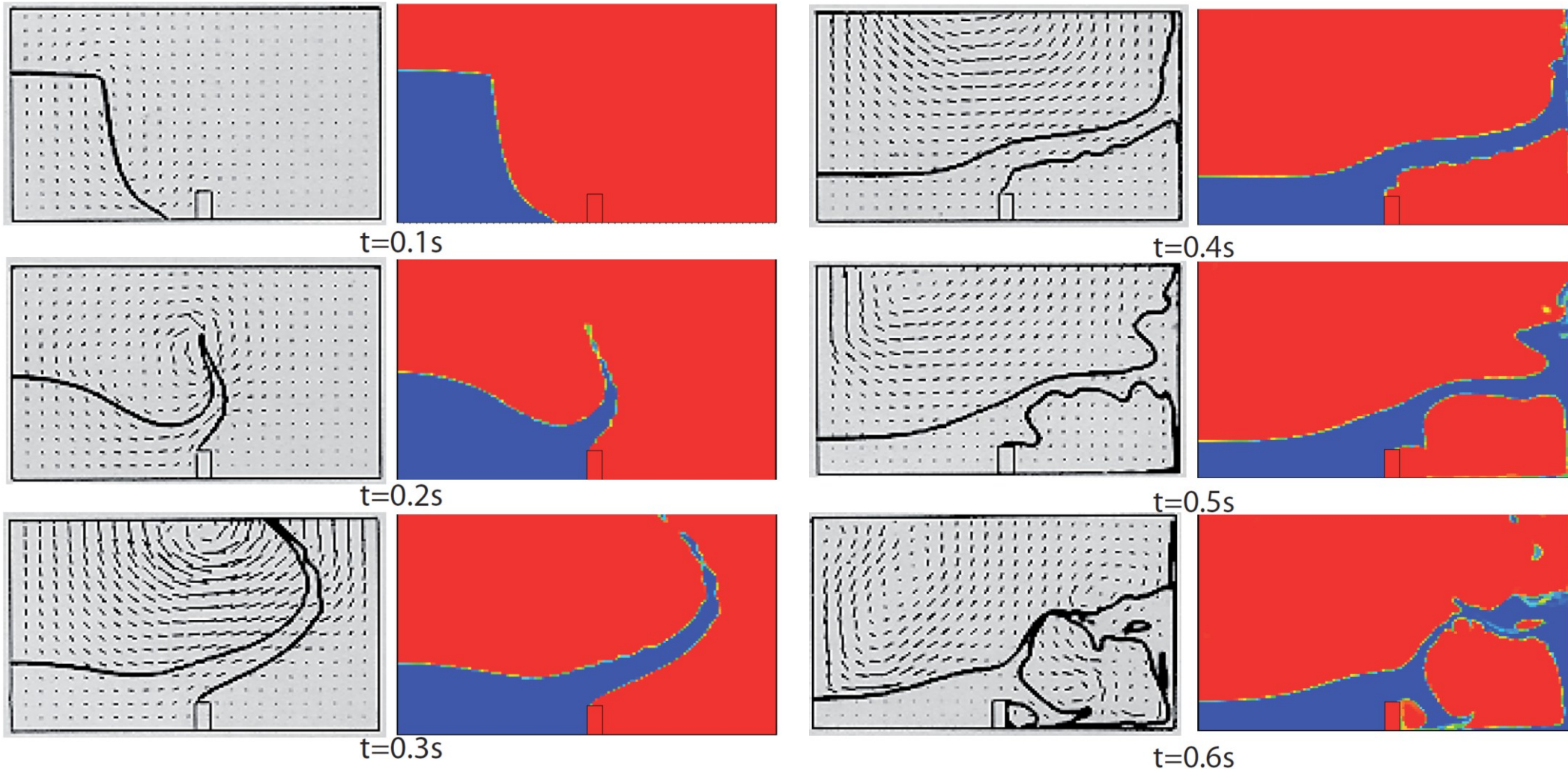
$$N_x = N_y = 150$$

$$\gamma_g = 1.4, \gamma_l = 7$$

$$\rho_0^g = 1.28 \text{ kg.m}^{-3}, \rho_0^l = 1000 \text{ kg.m}^{-3}$$

$$P_0 = 10^5, c_{\text{sound}} = 350 \text{ m.s}^{-1}$$

Collapse with an obstacle – comparison with incompressible fluid model



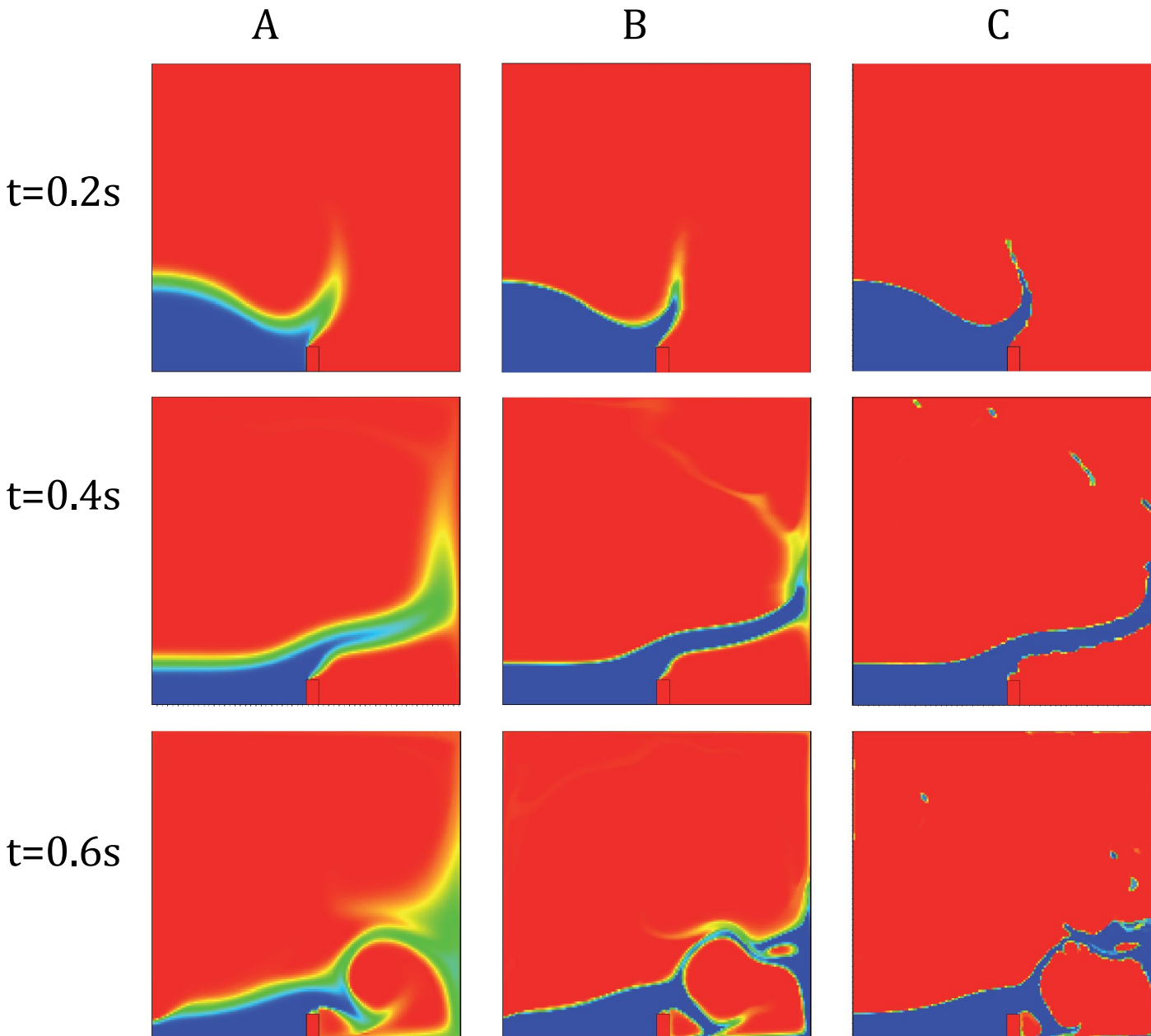
Num. Result.
Ubbink

Num. Result. with
Odyssey

Num. Result.
Ubbink

Num. Result. with
Odyssey

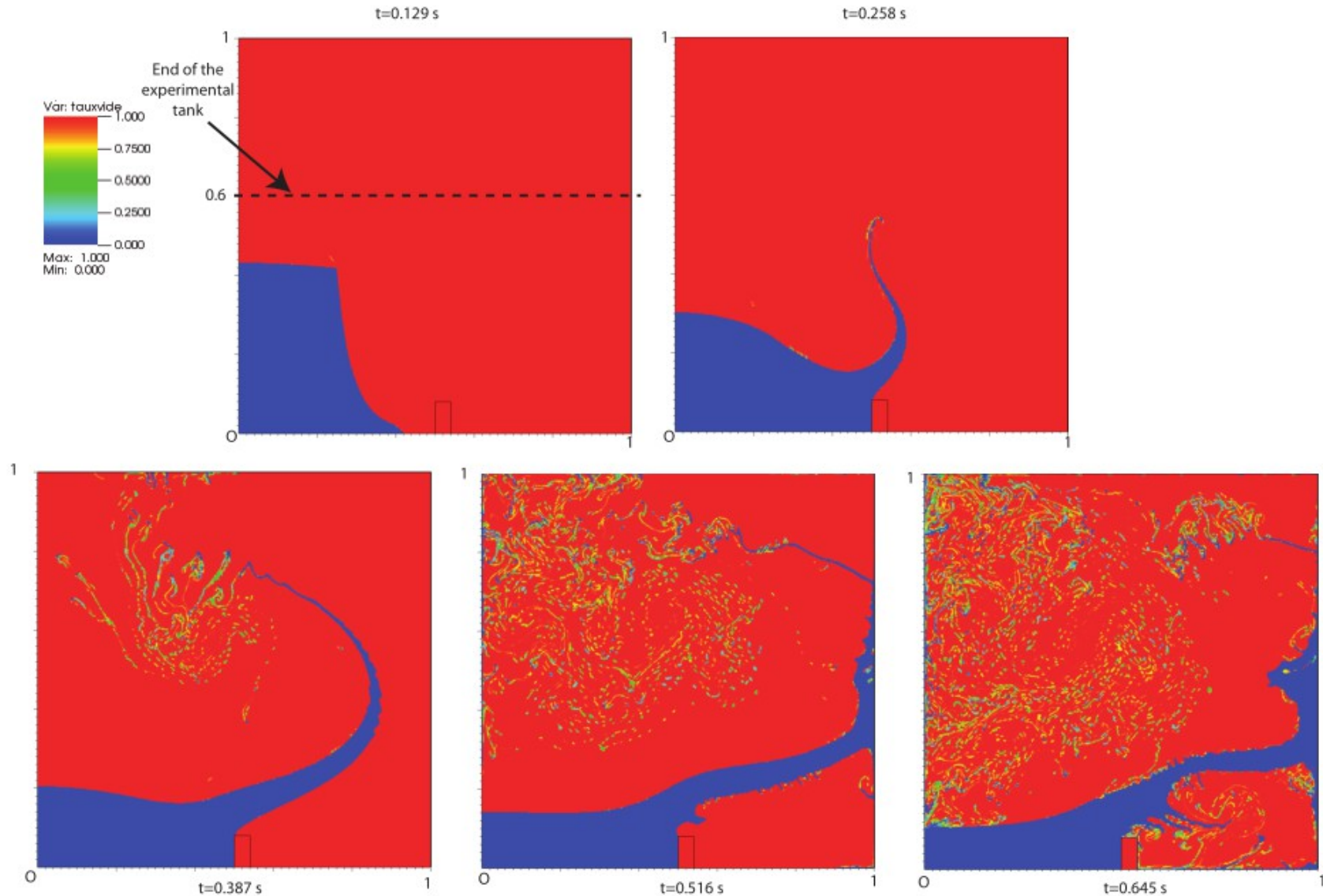
Benefits of the antidiffusive approach



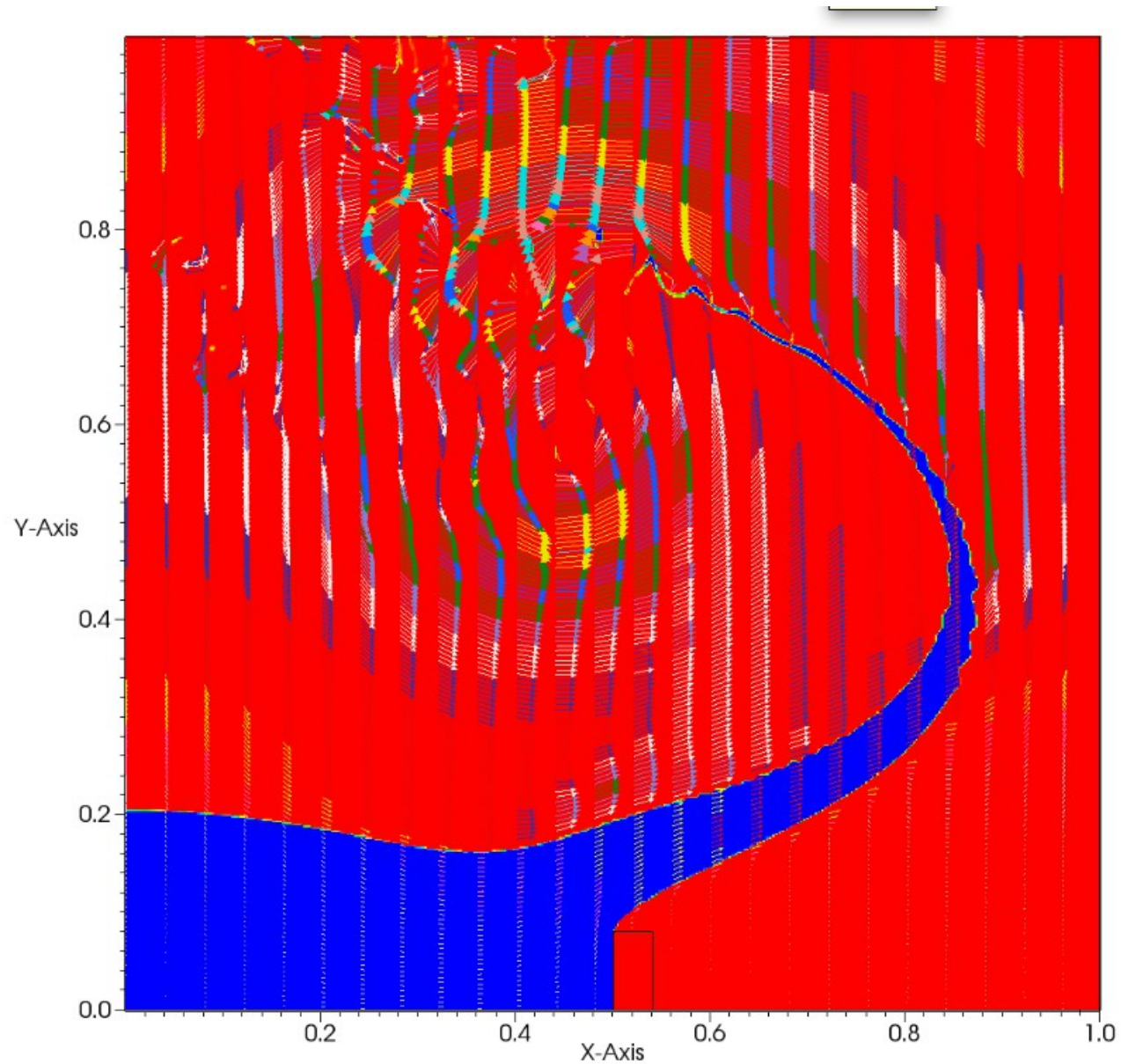
Evolution of ϕ for different remapping algorithms

- ✓ Case A: 1st order with upwind
- ✓ Case B: 2nd order with upwind
- ✓ Case C: 1st order with Low-Diff.

Gas mass fraction : numerical diffusion appears due to filamentation / fragmentation

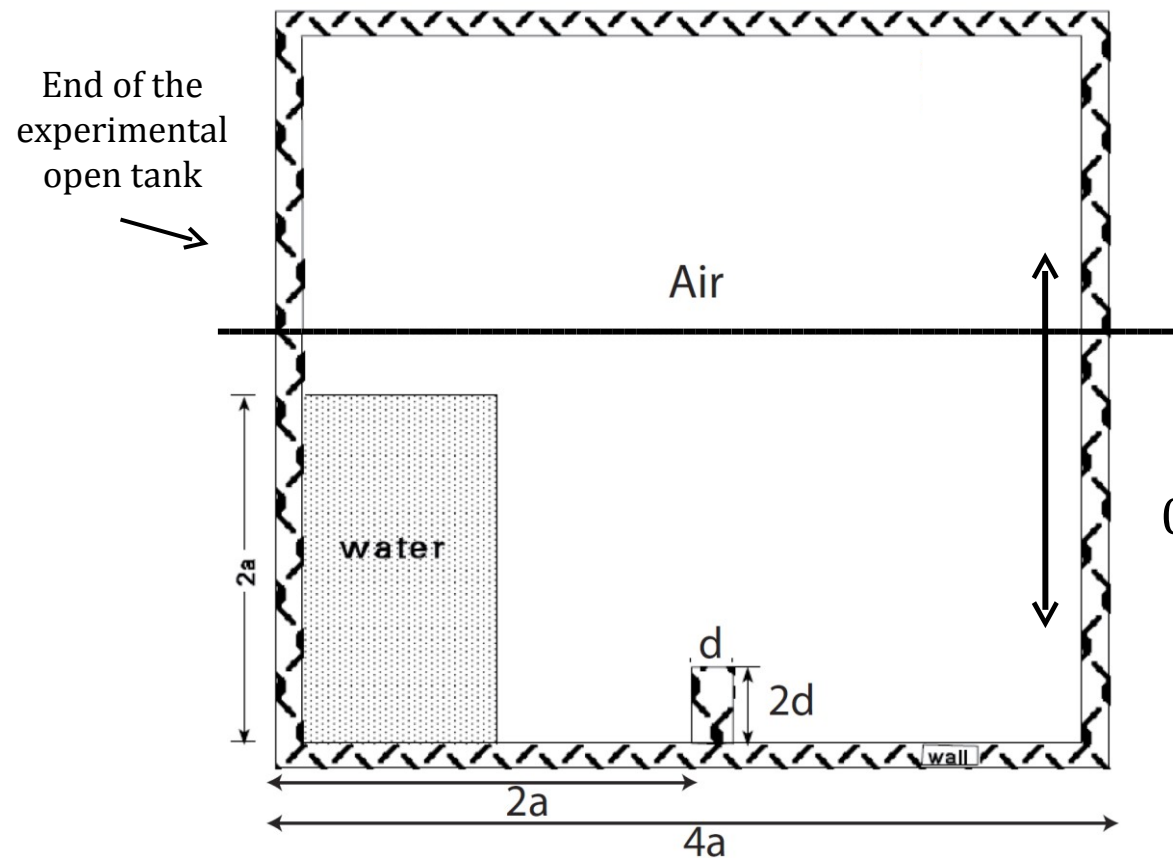


Velocity vector field



- Another case of collapse of a liquid column with an obstacle

D. M. Greeves Simulation of viscous water column collapse using adapting hierarchical grids J. Num. Meth. Fluids 2006



$$a = 0.25, d = 0.04$$

$$L_x = L_y = 1 \text{ m}$$

$$N_x = N_y = 300$$

$$\gamma_g = 1.4, \gamma_l = 7$$

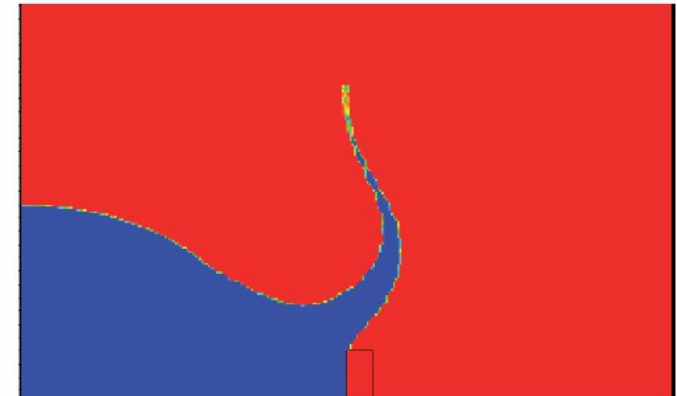
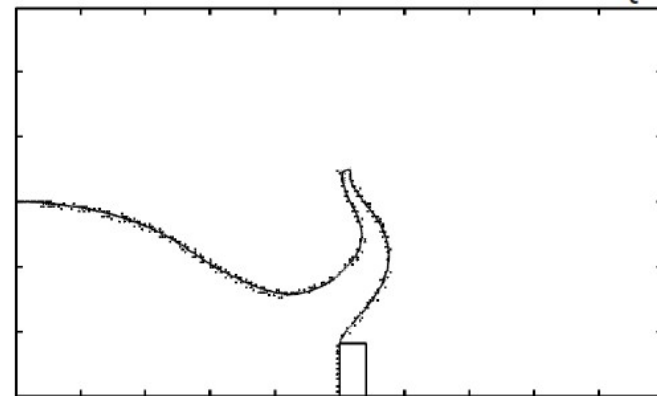
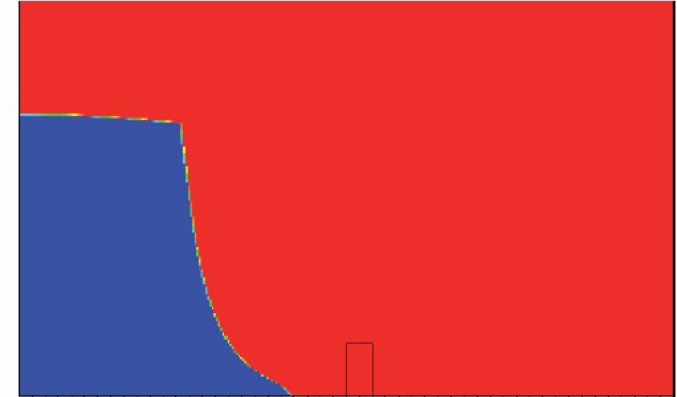
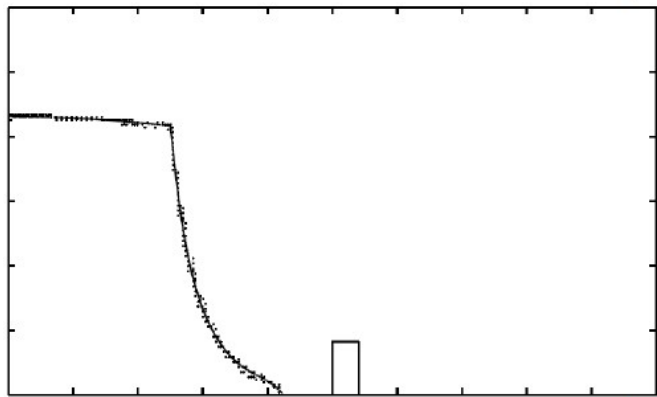
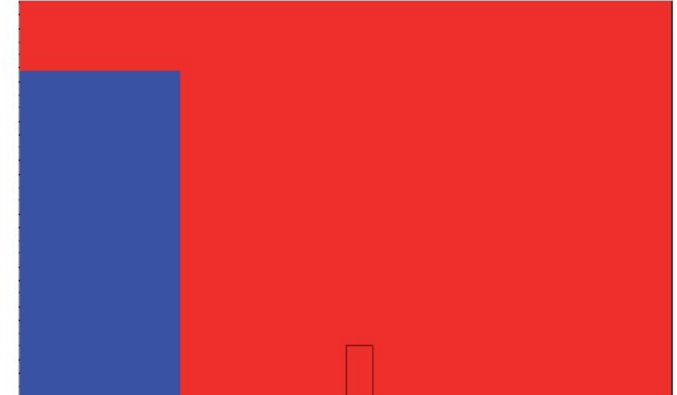
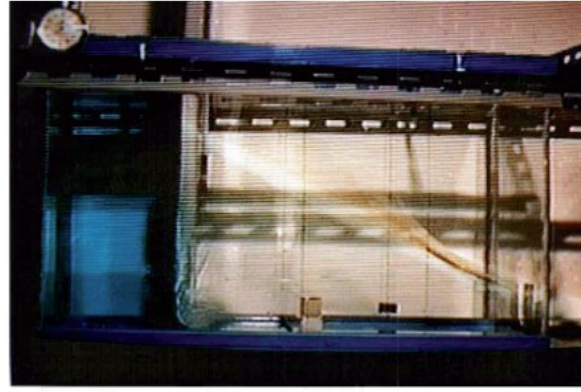
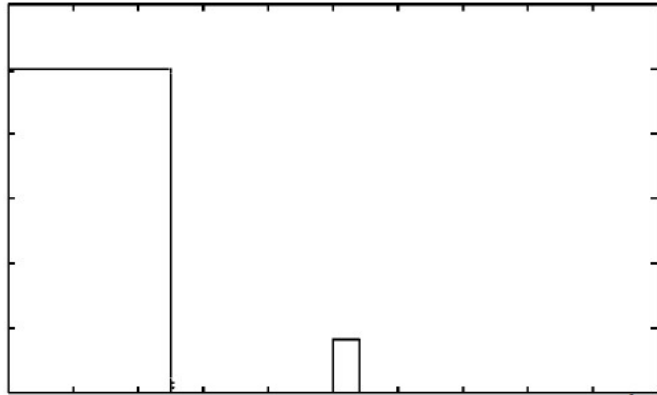
$$\rho_0^g = 1. \text{ kg.m}^{-3}, \rho_0^l = 1000 \text{ kg.m}^{-3}$$

$$P_0 = 10^5, c_{\text{sound}} = 350 \text{ m.s}^{-1}$$

Exp: from

Koshizuka et al A particle method.. Comp. Fluid Mech. 1995

Simulations of a dam break



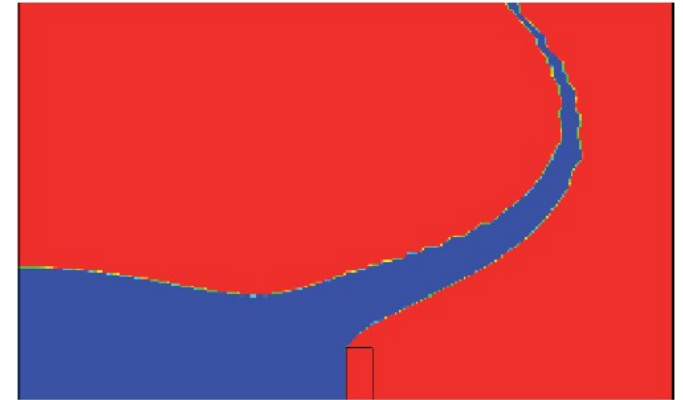
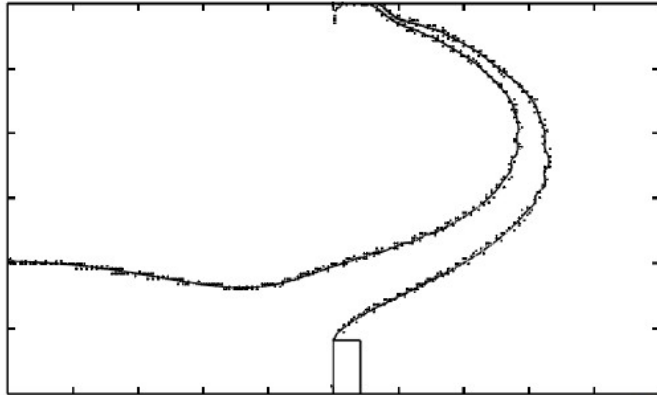
Sim. Greeves

$t=0.258s$

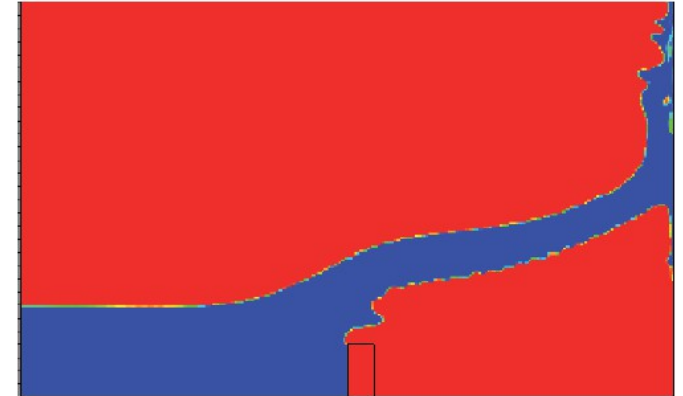
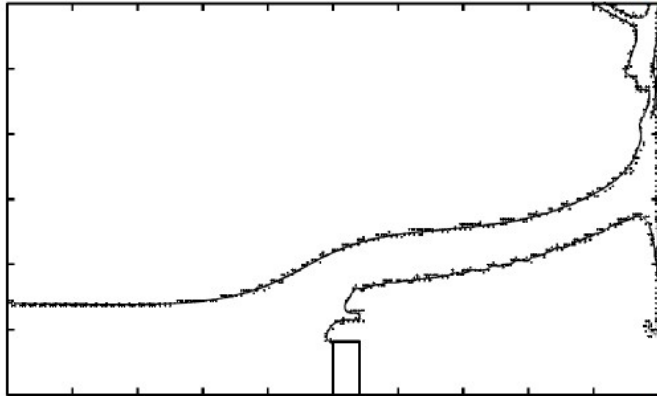
Exp. Koshizuka

Sim. Odyssey

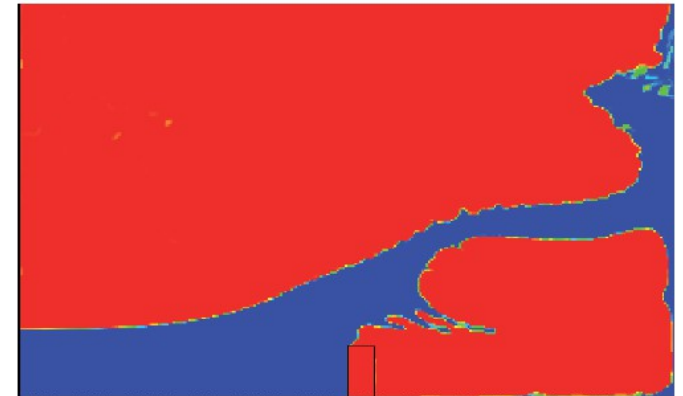
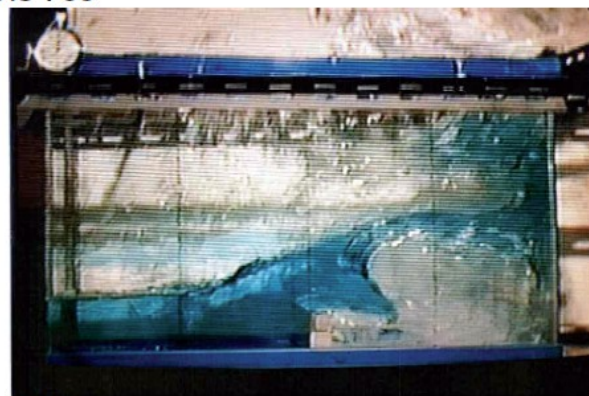
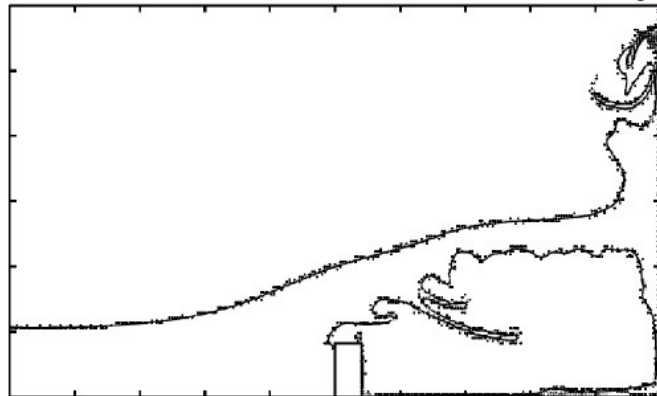
Simulations of a dam break



t=0.387s



t=0.516s



t=0.645s

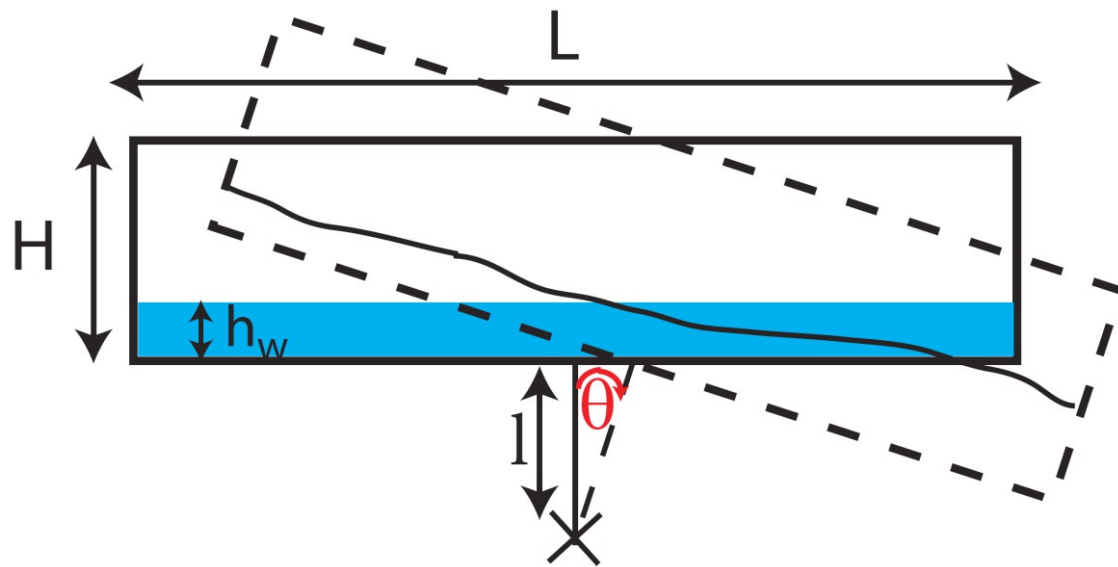
Sim. Greeves

Exp. Koshizuka

Sim. Odyssey

Sloshing test cases – pitch motion

- Sloshing due to the **pitch motion** of a rectangular tank:



J.R. Shao *et al.* An improved SPH method for modeling liquid sloshing dynamics. *Comp. Fluids* 2012

$$L = 0.64m, H = 0.14m, h_w = 0.03m$$

$$N_x = 300, N_y = 67$$

The tank is oscillating as a **pendulum** according to:

$$\theta(t) = \theta_0 \sin(\omega_r t)$$

with $\theta_0 = 6^\circ$, $\omega_r = 4.34 \text{ rad/s}$ ($T = 1.45 \text{ s}$)

Simulation are performed in the frame of reference of the tank.

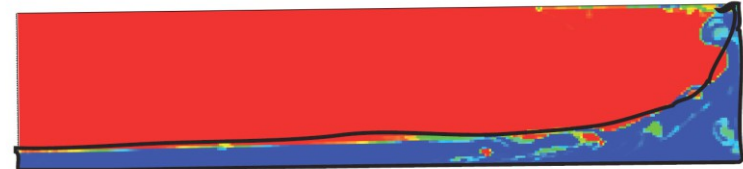
Sloshing test cases – pitch motion

We superimpose the profile of the article:

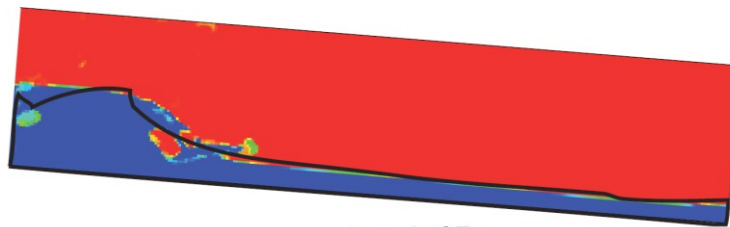
J.R. Shao *et al.* . An improved SPH method for modeling liquid sloshing dynamics. *Comp. Fluids* 2012



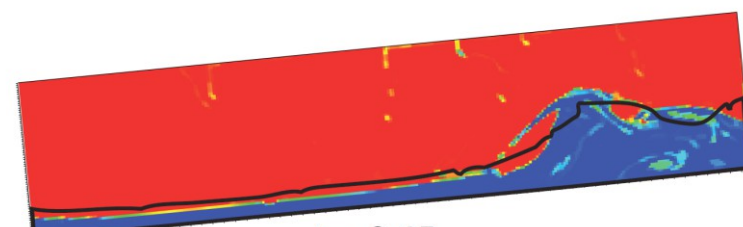
$t_1=1.45s$



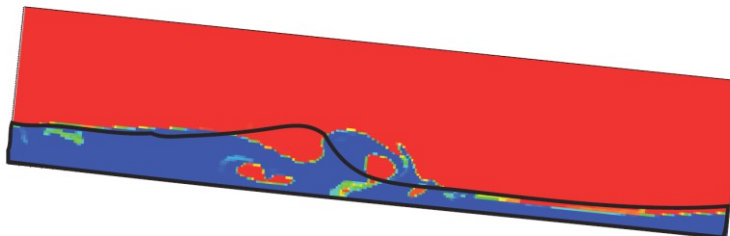
$t_5=2.2s$



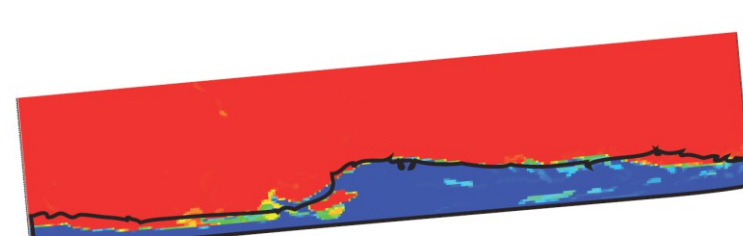
$t_2=1.65s$



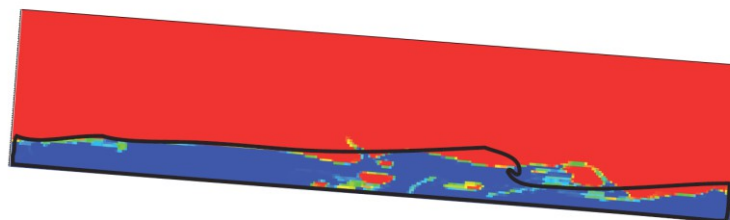
$t_6=2.45s$



$t_3=1.85s$



$t_7=2.65s$

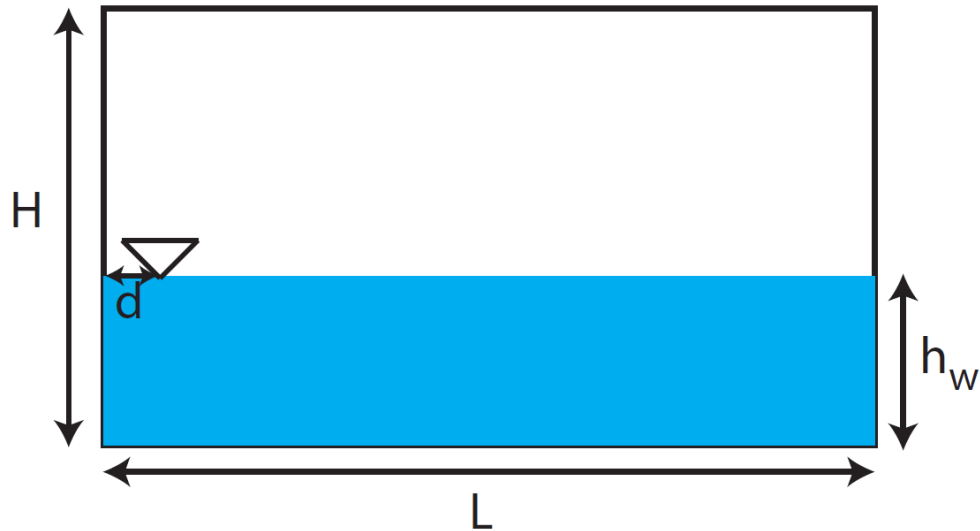


$t_4=1.98s$



$t_8=2.90s$

Sloshing due to the **surge motion** of a rectangular tank:



J.R. Shao *et al.* . An improved SPH method for modeling liquid sloshing dynamics. *Comp. Fluids* 2012

$$L = 1.73m, H = 1.15m, h_w = 0.6m$$

$$d = 0.05 \text{ m}$$

$$N_x = 173, N_y = 115$$

The tank is moving horizontally according to:

$$x(t) = A \cos\left(\frac{2\pi t}{T}\right)$$

with $A = 0.032 \text{ m}$, $T = 1.3 \text{ s}$ ($\omega_{forced} = 4.83 \text{ rad/s}$).

First natural frequency of the fluid in the box

$$\omega_{fluid} = \sqrt{g \frac{\pi}{L} \tanh\left(\frac{\pi}{L} h_w\right)} \approx 3.77 \text{ rad/s}$$

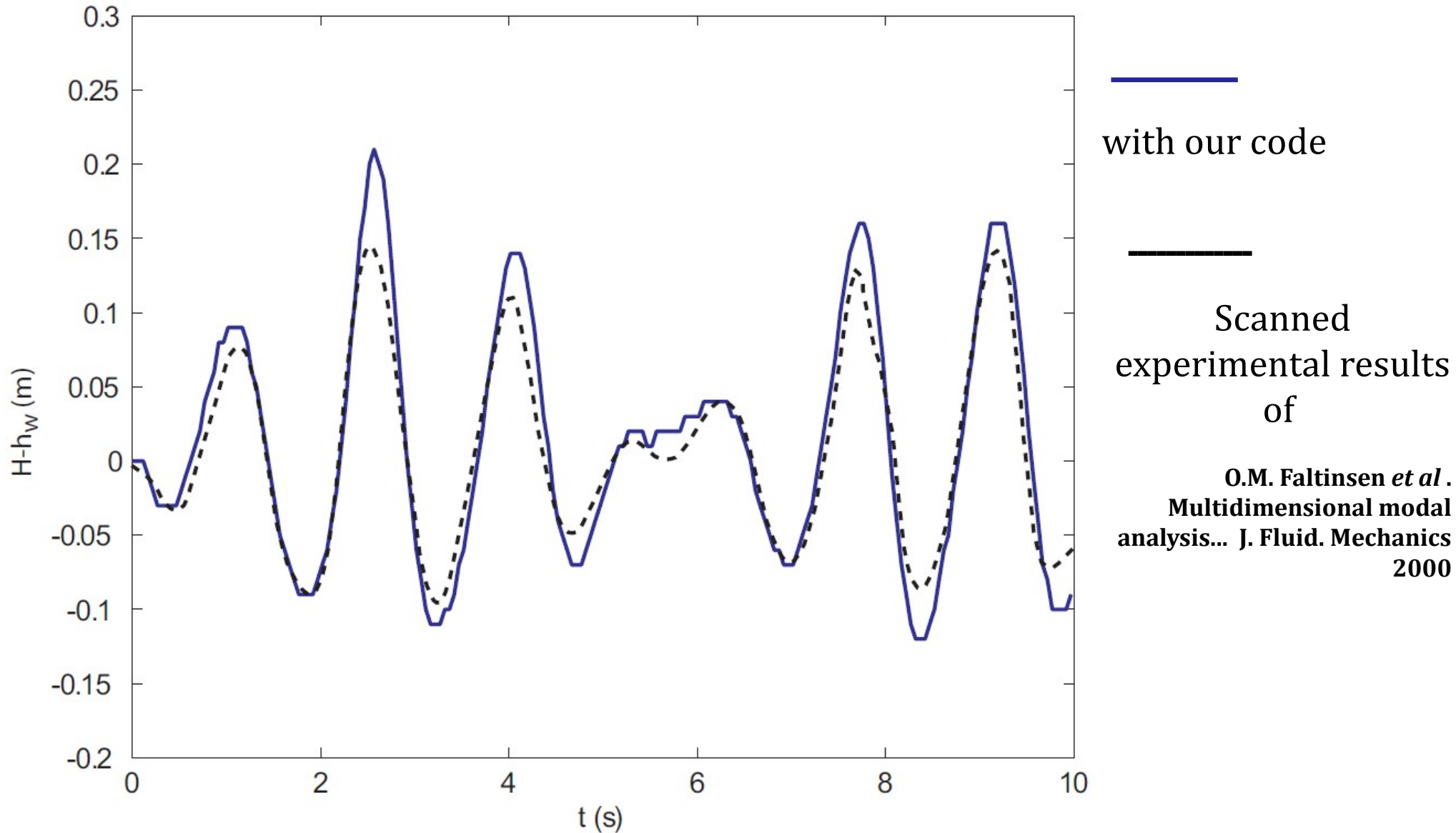
Two frequencies are acting ω_{fluid} and ω_{forced}

Experimental results available:

O.M. Faltinsen *et al.* . Multidimensional modal analysis... *J. Fluid. Mechanics* 2000

Sloshing test cases – surge motion

Free surface elevation of water at the probe



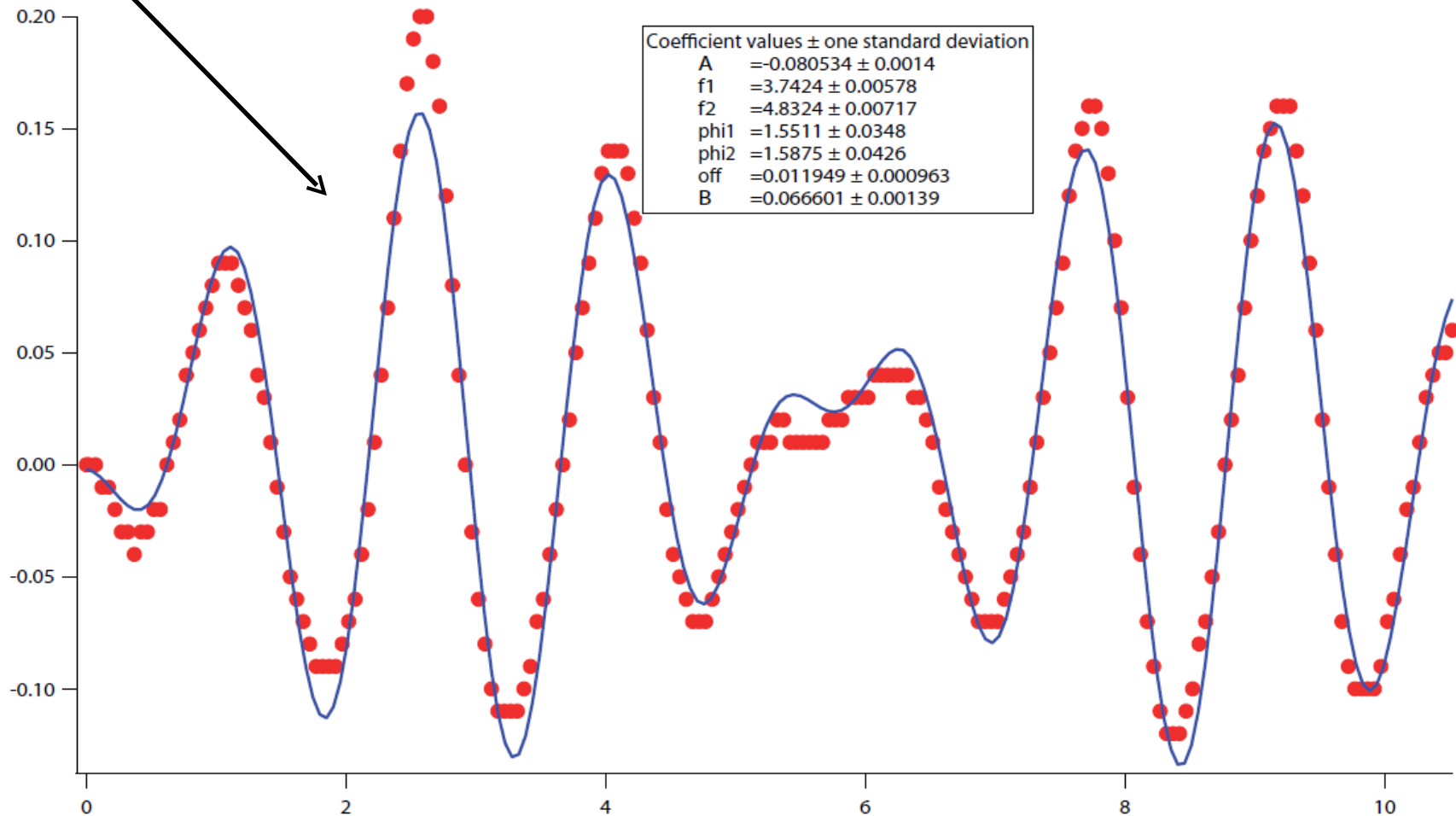
Sloshing test cases – Surge motion

We search to **find a fit** of our curve with a function as a superposition of two signals

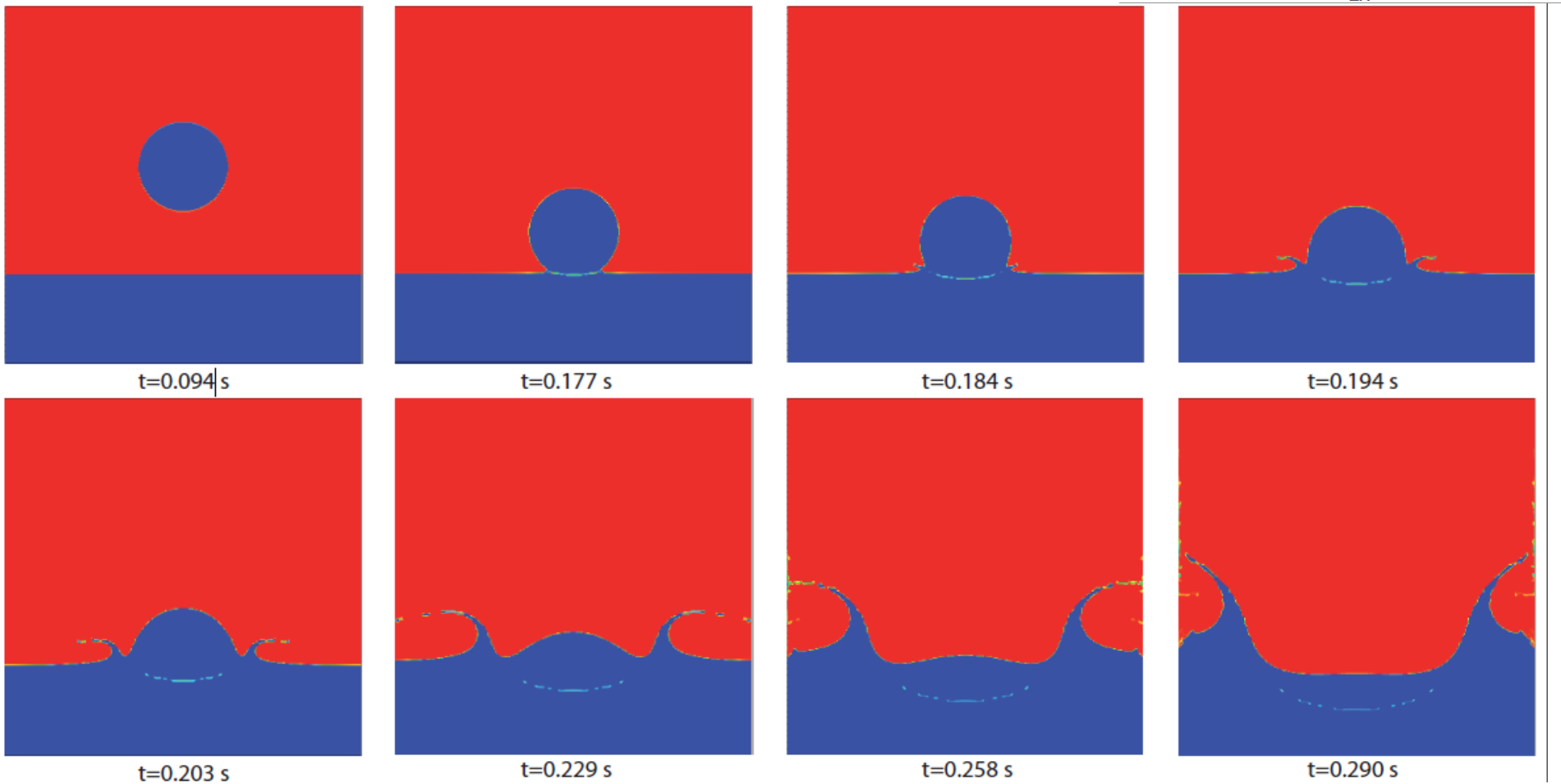
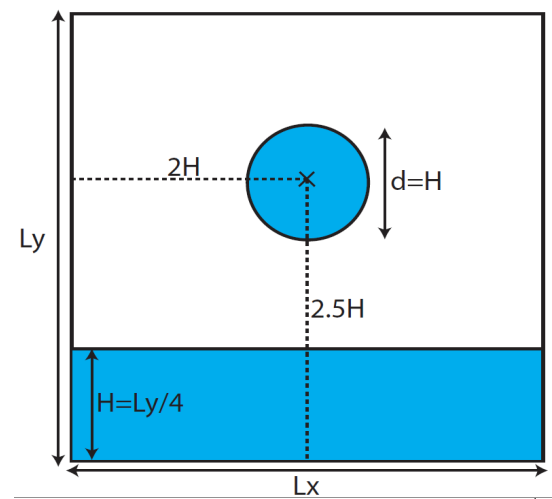
$$f(t) = A_1 \sin(f_1 t + \varphi_1) + A_2 \sin(f_2 t + \varphi_2)$$

we get: $f_1 = 3.74 \pm 0.01$ rad/s, $f_2 = 4.83 \pm 0.01$ rad/s

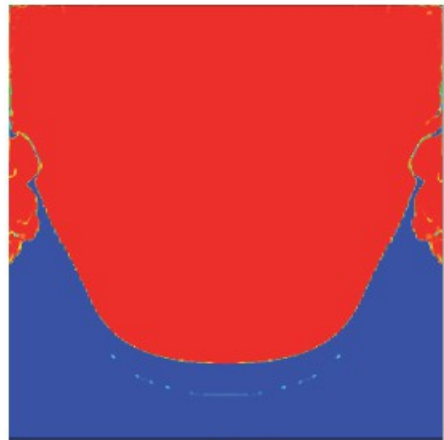
very close to $\omega_{\text{fluid}} \approx 3.77$ rad/s and $\omega_{\text{forced}} = 4.83$ rad/s



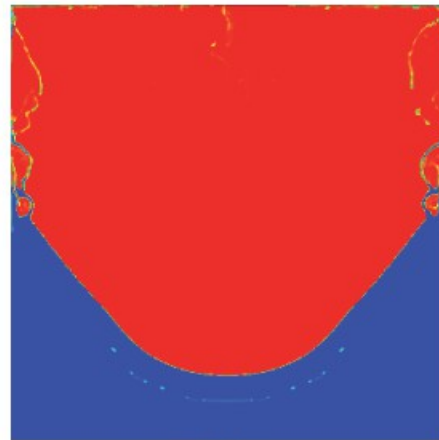
Free fall of liquid and impact with liquid at rest



Liquid-liquid impact



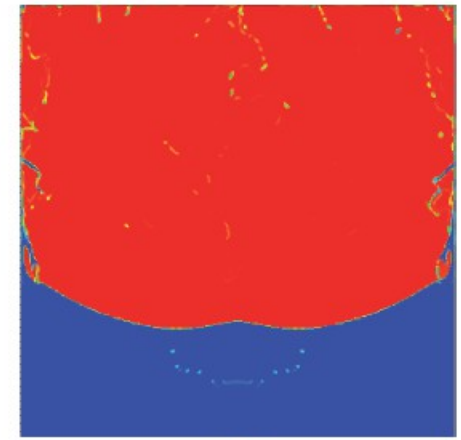
$t=0.349$ s



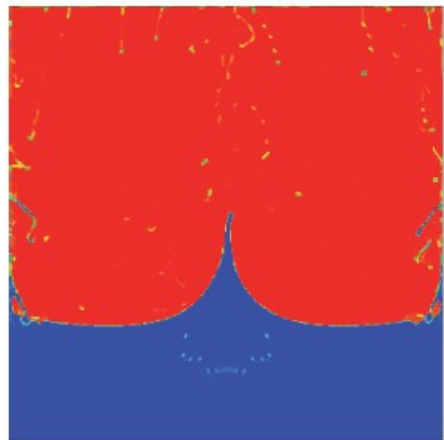
$t=0.450$ s



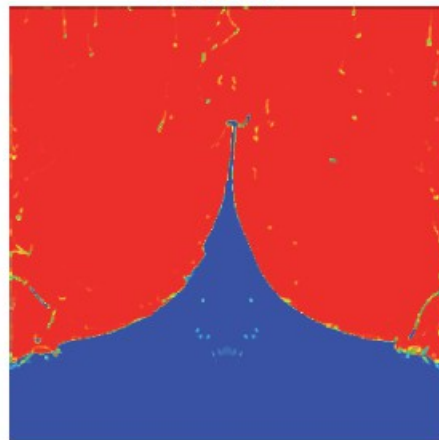
$t=0.545$ s



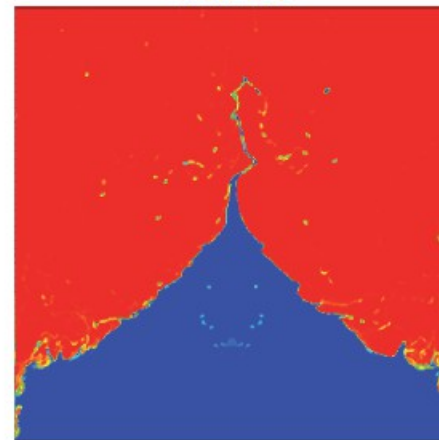
$t=0.564$ s



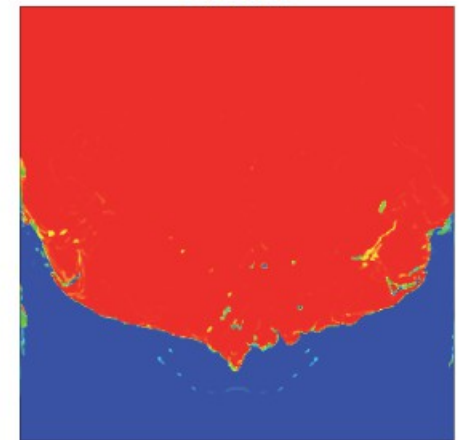
$t=0.618$ s



$t=0.694$ s

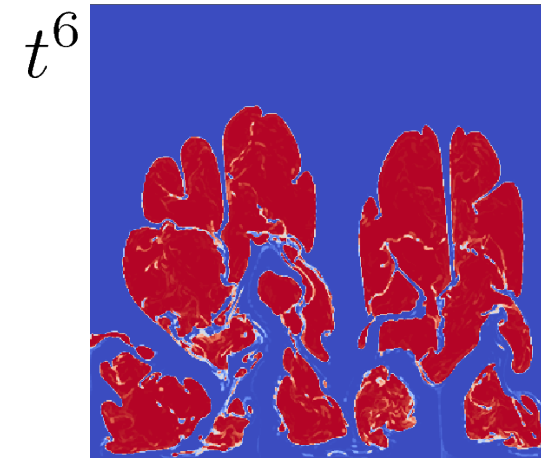
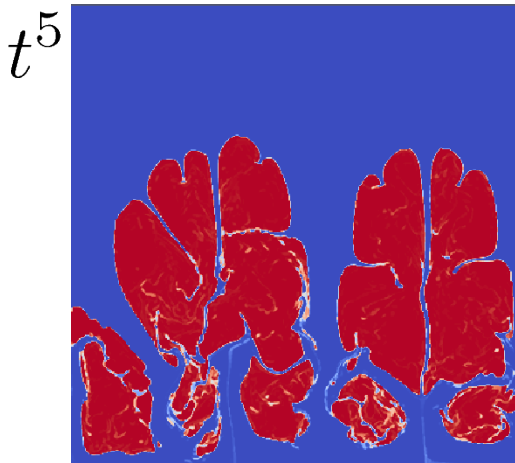
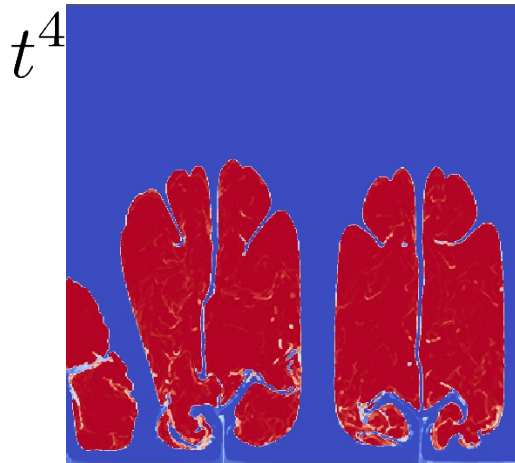
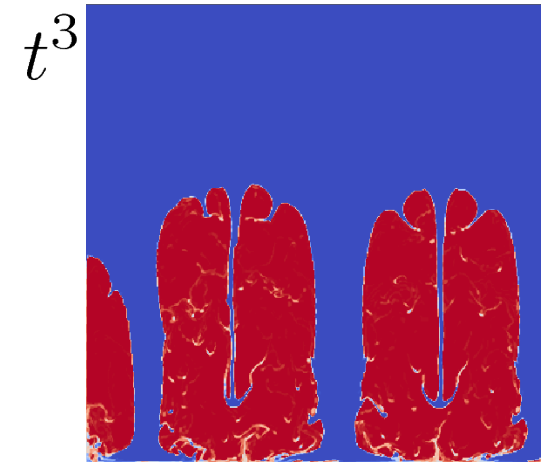
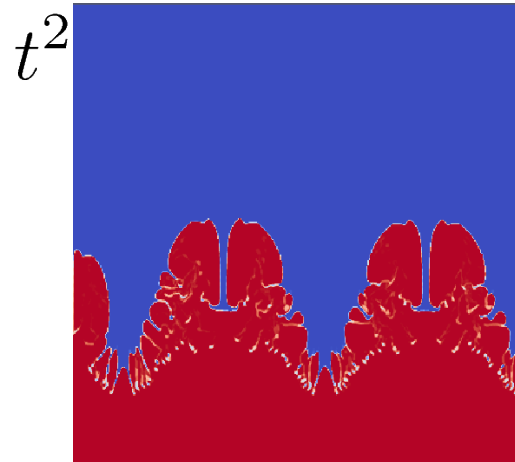
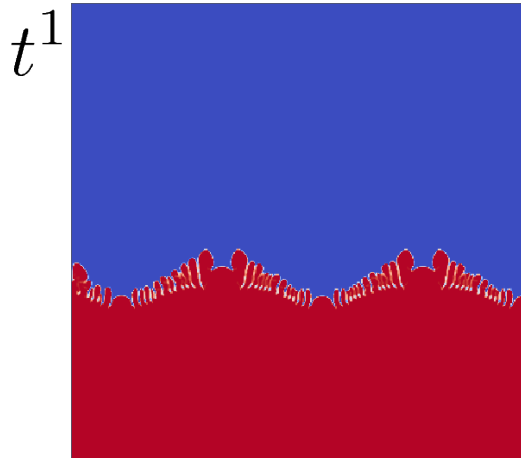
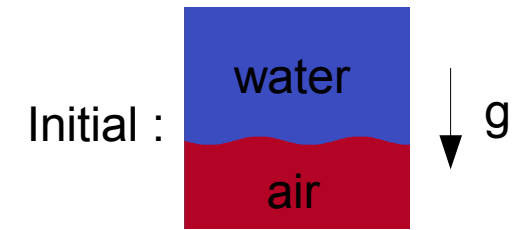


$t=0.859$ s



$t=1.055$ s

LT air-water Rayleigh-Taylor instability



About 0.5 sec of physical time

Grid 400x400, about 1.5 day of computation (sequential)

Concluding remarks

- Innovative numerical Eulerian method involving :
 - a Lagrange-Remap finite volume method
 - an anti-diffusive approach on the gas mass/volume fraction
- The test cases show a good agreement between XP and other codes (dam break, sloshing events)
- Ongoing works : XP + num of water wave wall impact (L. Lenain, K. Melville, U. Delaware, Frédéric Dias, U. College Dublin).
- Need to add : physical viscosity, surface tension
- Graphics Processing Unit (GPU) implementation

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Thank you for your attention

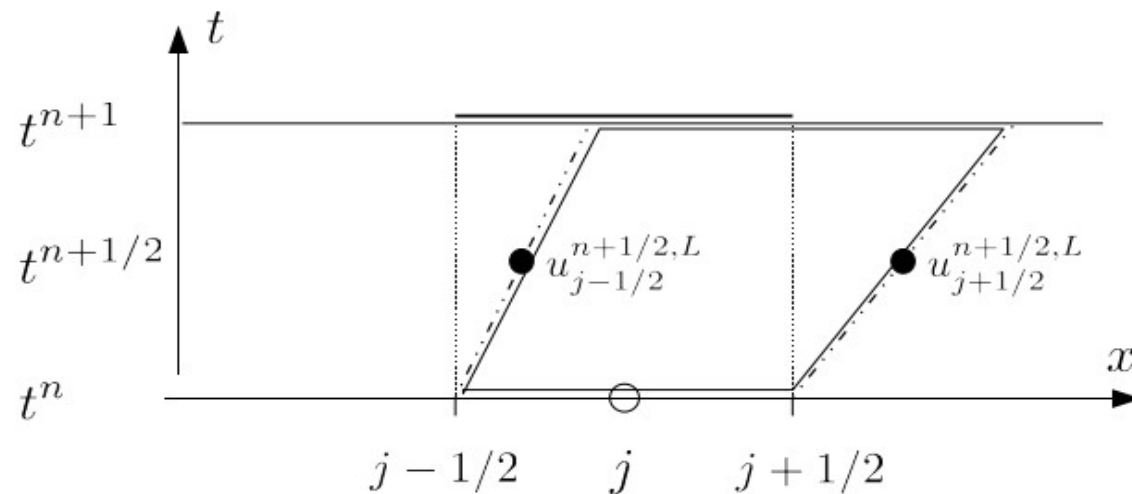
Lagrange-remap : conservative reformulation

i.e.

$$\rho_j^{n+1,L} = \frac{\rho_j^n}{1 + \frac{\Delta t}{h} (\Delta u)_j^{n+1/2,L}}, \quad (\Delta u)_j^{n+1/2,L} := u_{j+1/2}^{n+1/2,L} - u_{j-1/2}^{n+1/2,L}.$$

Projection step:

$$\rho_j^{n+1} = \frac{1}{h} \int_{I_j} \mathcal{I} \rho^{n+1,L}(x) dx = \frac{1}{h} \int_{I_j^{n+1,L}} \dots - \dots + \dots .$$



Lagrange-remap: conservative reformulation

Mass balance rewriting : under some convenient CFL condition, we have

$$\begin{aligned} h\rho_j^{n+1} &= h_j^{n+1,L} \rho_j^{n+1,L} - \Delta t \rho_{j+1/2}^{upw,n+1} u_{j+1/2}^{n+1/2,L} + \Delta t \rho_{j+1/2}^{upw,n+1} u_{j-1/2}^{n+1/2,L} \\ &= h\rho_j^n - \Delta t \rho_{j+1/2}^{upw,n+1} u_{j+1/2}^{n+1/2,L} + \Delta t \rho_{j+1/2}^{upw,n+1} u_{j-1/2}^{n+1/2,L} \end{aligned}$$

in the form

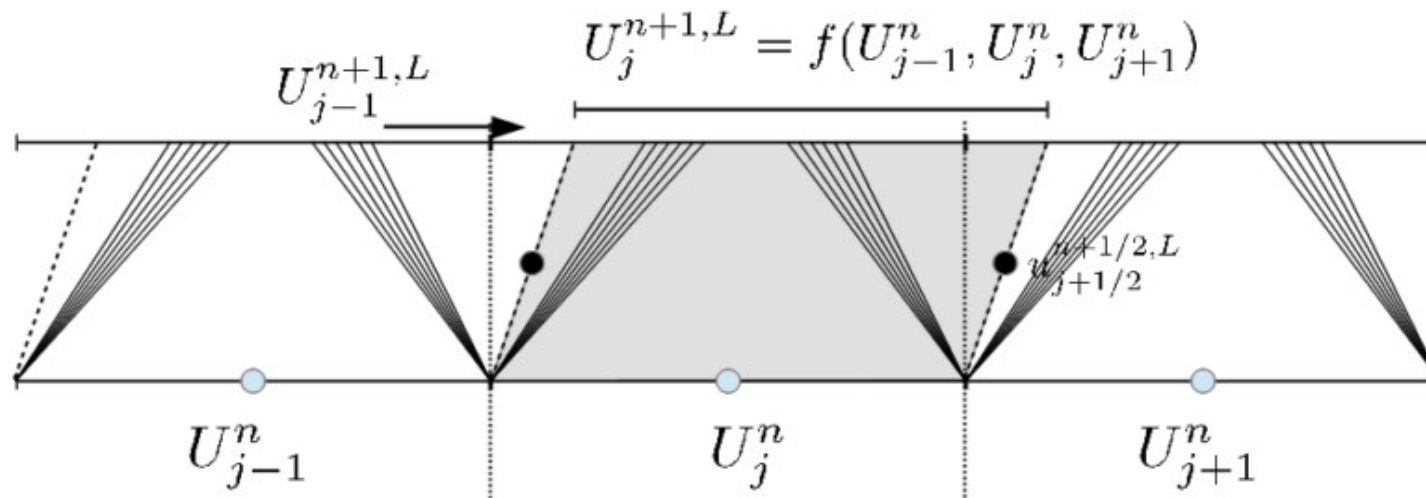
$$\rho_j^{n+1} = \rho_j^n - \frac{\Delta t}{h} \left(\Phi_{m,j+1/2}^{n+1/2,n+1} - \Phi_{m,j-1/2}^{n+1/2,n+1} \right),$$

$$\Phi_{m,j+1/2}^{n+1/2,n+1} = \rho_{j+1/2}^{upw,n+1} u_{j+1/2}^{n+1/2,L}.$$

[De Vuyst, Fochesato, Loubère, Saas, Motte, Ghidaglia, preprint paper 2013]

Remark

First-order (1st-order remap) LR schemes are actually 5-point schemes !

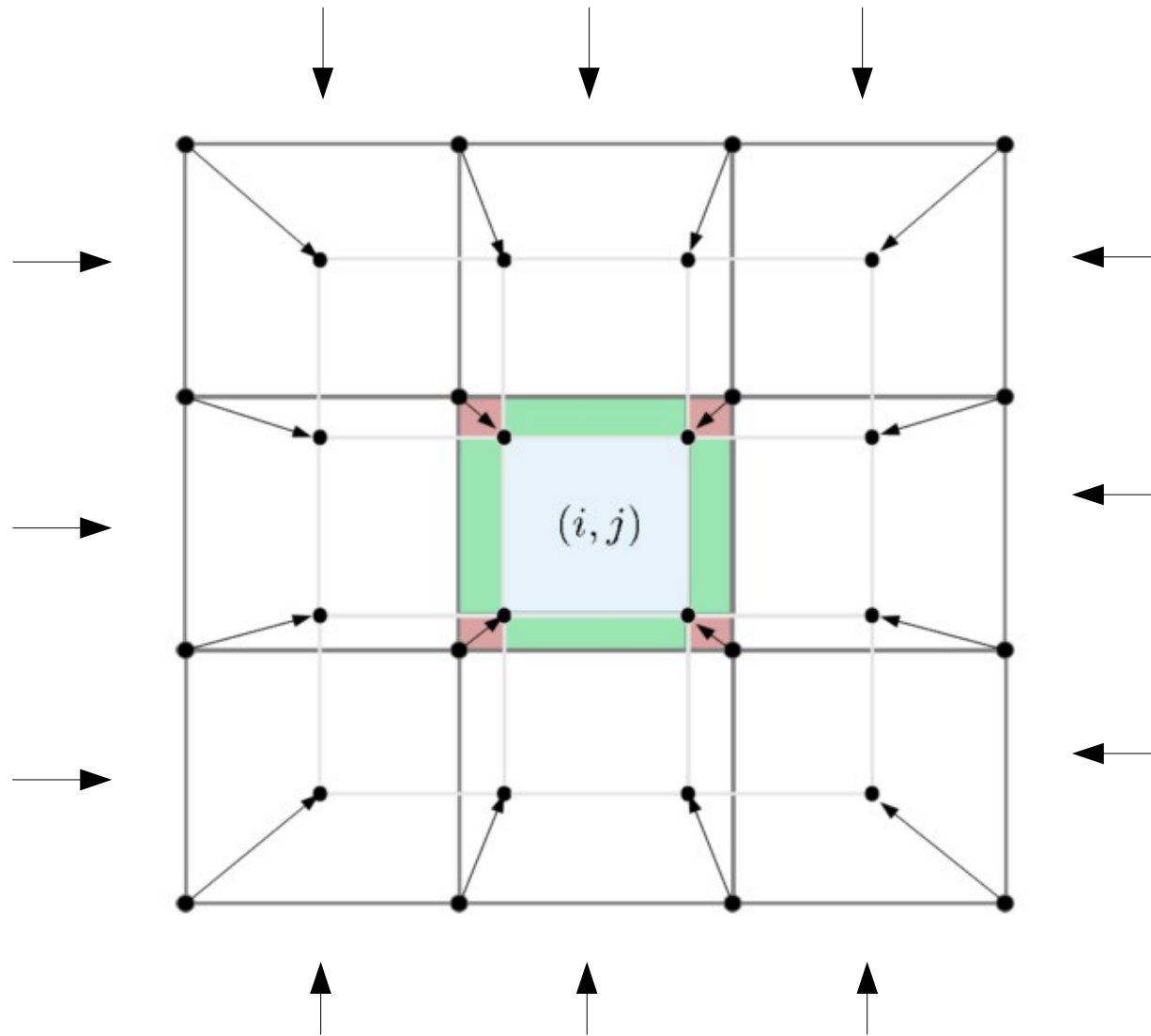


$$U_j^{n+1} = U_j^n - \frac{\Delta t}{h} \left(\Phi_{j+1/2}^{n,n+1} - \Phi_{j-1/2}^{n,n+1} \right),$$

$$\Phi_{j+1/2}^{n,n+1} = \Phi \left(U_{j-1}^n, U_j^n, U_{j+1}^n, U_{j+2}^n, \Delta t \right).$$

→ Large stencil method : limited GPU performance because of lot of memory reads.

Lagrange-remap : two-dimensional case (1st-order accurate)



21-point scheme ! (large stencil)
NB : multidimensional corner effects